

## **Development of a formulation platform for a spray-dried, inhalable tuberculosis vaccine candidate**

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### **ABSTRACT**

Protection against primarily respiratory infectious diseases, such as tuberculosis (TB), can likely be enhanced through mucosal immunization induced by direct delivery of vaccines to the nose or lungs. A thermostable inhalable dry powder vaccine offers further advantages, such as independence from the cold chain. In this study, we investigate the formulation for a stable, inhalable dry powder version of an adjuvanted subunit TB vaccine candidate ID93+GLA-SE, containing recombinant fusion protein ID93 and glucopyranosyl lipid A (GLA) in a squalene emulsion (SE) as an adjuvant system, via spray drying. The addition of leucine (20% w/w), pullulan (10%, 20% w/w), and trileucine (3%, 6% w/w) as dispersibility enhancers was investigated with trehalose as a stabilizing agent. Particle morphology and solid state, nanoemulsion droplet size, squalene and GLA content, ID93 presence, and aerosol performance were assessed for each formulation. The results showed that the addition of leucine improved aerosol performance, but increased aggregation of the emulsion droplets was demonstrated on reconstitution. Addition of pullulan preserved emulsion droplet size; however, the antigen could not be detected after reconstitution. The trehalose-trileucine excipient formulations successfully stabilized the adjuvant system, with evidence indicating retention of the antigen, in an inhalable dry powder format suitable for lung delivery.

**Key words: spray drying, tuberculosis vaccine, inhalable delivery, nanoencapsulation, particle engineering, dispersibility.**

# 1 Introduction

Spray drying is a method of desiccating a liquid product into a dry powder composed of many small particles. Briefly, a liquid feedstock is atomized into small droplets during spray drying. These droplets, containing dissolved or suspended solids, evaporate within a drying gas into particles. The particles are then separated from the flow, e.g. with a cyclone. Spray drying is commonly used in the food processing and pharmaceutical industries to encapsulate an active component into a dry powder and thus protect it from potentially harmful environmental conditions, such as high humidity and temperature [1]. Spray drying has been previously used to improve the stability of experimental vaccines using the disaccharide trehalose as a stabilizer [2, 3, 4, 5]. Spray drying also allows for engineering of the resulting particles for specific properties, making them suitable for intranasal or pulmonary routes via inhalation [6, 7, 8]. Both the improvement of thermostability and the development of an inhalable route of delivery may be applied to vaccines to improve their accessibility.

Preclinical trials of dry powder vaccines have been promising. However, as dry powder vaccination via inhalation is an emerging field, clinical trials are limited. The first inhalable dry powder vaccine for pulmonary delivery, a measles vaccine, completed Phase I clinical trials in 2013 [9]. Further work is warranted because there are many benefits to developing alternative administration routes to injection. The general advantages of respiratory drug delivery include convenience, reduced chance of adverse systemic reactions, and smaller amounts of drug required due to direct targeting. Compared to injectable delivery, the use of a non-invasive route of administration reduces the chance of needlestick injuries, and with that reduces the transmission of blood-borne illnesses such as HIV. Additionally, injectable delivery of a reconstituted vaccine requires sterile water, a commodity that is taken for granted in developed nations. Furthermore, mucosal immunization through inhalable delivery is potentially more effective at conferring protection than parenteral injection against respirable diseases, such as tuberculosis (TB) [10].

TB is the leading cause of death from a single infectious agent, and approximately 10 million people contracted TB in 2018 [11]. TB is transmitted through air as droplets, making the lungs the primary

infection site [12]. Currently, the bacille Calmette-Guérin (BCG) vaccine is the only licensed TB vaccine. BCG is administered via injection as part of standard childhood immunization programs in many countries [11]. Due to the widespread use of BCG, any improvement in efficacy would have a large impact. To this end, administration routes alternative to injection have been investigated for BCG. Research involving animal models have reported that the BCG vaccine provides better protection against TB when administered to the respiratory system directly rather than through injection [13, 14, 10, 15]. Aguilo et al. [10] demonstrated that intranasal delivery of BCG, but not subcutaneous delivery, conferred protection against pulmonary TB in TB-susceptible mice. Verreck et al. [15] suggested that pulmonary immunization results in a more reliably protective local immune response. Recently, Price et al. [6] spray-dried the BCG vaccine into a thermostable presentation designed for inhalable dry powder delivery. Mouse immunization studies showed that the liquid BCG vaccine, the reconstituted freshly spray-dried BCG vaccine, and the reconstituted spray-dried BCG vaccine stored at 25 °C for two years had no significant difference in induced cytokine response in mice. However, despite the effort in improving the efficacy of BCG vaccine via different routes of delivery, the vaccine carries several limitations. It has demonstrated variable efficacy in humans based on geography (0-80%) [16], confers only limited protection to adults [11], is unsafe for immunocompromised infants [17], and is not effective in preventing latent TB from becoming active [11]. Alternative vaccines for TB are being developed to address these shortcomings.

One such vaccine candidate is ID93+GLA-SE, an adjuvanted subunit vaccine comprised of a recombinant fusion antigen, ID93, and an adjuvant system, GLA-SE. The main components of the adjuvant system consist of synthetic TLR4 agonist glucopyranosyl lipid A (GLA), squalene nanodroplets, and DMPC as an emulsifier. ID93+GLA-SE has shown promising results in animal models [18] and has progressed to Phase II clinical testing [11]. Conversion of this vaccine to a thermostable presentation has been explored, as per WHO guidelines, to focus on thermostable options for promising candidates [19, 20]. Both lyophilization [21, 22] and spray drying [23] have been investigated as desiccation methods and were found to confer thermostability to ID93+GLA-SE. The lyophilized vaccine candidate is currently undergoing a Phase I

clinical trial [24]. Spray drying was investigated as an alternative method as it is considered more scalable than lyophilization, potentially has lower processing costs [25, 26], and also allows for the manipulation of morphology and structure of the final particle product. Previous work spray-drying ID93+GLA-SE focused on the development and stability of a presentation designed for eventual reconstitution and injection that utilized only trehalose as a stabilizing excipient [23]. The promising results demonstrated by the spray-dried presentation prompted investigation into spray drying an inhalable presentation of ID93+GLA-SE.

Respiratory delivery of an aerosolized powder occurs through nasal or pulmonary routes, each with an optimum particle size range for the most effective drug delivery. Drug particles or drug sprays are usually delivered locally during nasal administration, whereas the active components for pulmonary delivery must surpass the upper extrathoracic airways before it can deposit in either the targeted trachea-bronchia region or the targeted alveolar region [27]. Therefore, successful pulmonary delivery requires smaller particles (1-5  $\mu\text{m}$ ) than for nasal delivery ( $\sim 20 \mu\text{m}$ ) and much more flowable drug particles that need to be carefully designed [28, 29, 30, 31]. In addition, to achieve successful lung deposition, particles must also not get stuck in the delivery device, or be exhaled out. Therefore, the formulation development for pulmonary delivery can be much more challenging. Two of the most important factors that need to be considered during dry powder formulation development are the aerodynamic particle size and dispersibility of the powder [32]. However, delivery devices, such as dry powder inhalers (DPI), are usually unable to fully disperse the powder due to the intrinsic cohesiveness of the powder. The addition of larger carrier particles is a traditional method to reduce powder retention within DPIs. However, added carriers should be used only for potent actives as they reduce the drug load per inhaled dose. Instead, particle engineering can be used to improve powder dispersibility through the addition of dispersibility enhancing agents such as leucine, pullulan, and trileucine.

Leucine is an amino acid that has been proposed in combination with trehalose as a system to stabilize biologics [33]. The leucine component of spray-dried formulations has been designed to form a fully crystalline, rugose outer shell to improve the dispersibility of a powder [34, 35]. Pullulan is a polysaccharide

that has been used in the food drying industry and pharmaceutical industry to improve thermostability. Films formed from drying pullulan with trehalose have been reported to improve the thermostability of live-attenuated or inactivated viral vaccines for up to 12 weeks at 40 °C [36]. Under normal spray drying conditions, both pullulan and trehalose remain amorphous [37]. Trileucine is a tripeptide that has been shown to form an amorphous layer on spray-dried particles under normal spray drying conditions [38]. The formation of a trileucine layer has been shown to reduce particle cohesiveness and thus improve aerosol performance [39]. The addition of trileucine has also been shown to improve the stability of trehalose microparticles suspended in HFA227ea propellant [40] and the stability of spray-dried bacteriophages [41].

Improved thermostability and development of an inhalable route would be especially beneficial for intervention of TB. This paper studies three dispersibility enhancers: leucine, pullulan and trileucine, for producing spray-dried ID93+GLA-SE powder suitable for inhalation. Success of the inhalable candidates was assessed in terms of aerosol performance and preservation of vaccine integrity after spray drying.

Characterization of vaccine integrity included testing for changes in emulsion size distribution, squalene and GLA content, and presence of ID93.

## 2 Materials and Methods

### 2.1 Materials

#### 125 Chemicals

Trehalose dihydrate with a purity of 98% was used as the primary stabilizing excipient for spray drying (CAS 6138-23-4; Fisher Scientific Ottawa, ON, Canada). L-Leucine with a purity of 99% (CAS 61-90-5; Fisher Scientific Ottawa, ON, Canada), pullulan (CAS 9057-02-7; Alfa Aesar, Tewksbury, MA, USA), and trileucine with a purity of  $\geq 90\%$  (CAS 10329-75-6; Sigma Aldrich, Oakville, ON, Canada) were investigated as dispersibility enhancing materials. Tris(hydroxymethyl)aminomethane (Tris) (CAS 77-86-1; Sigma Aldrich, Oakville, ON, Canada) and hydrochloric acid (CAS 7647-01-0; Sigma Aldrich, Oakville, ON, Canada) were used as a buffer system to adjust the pH of the feedstock prior to spray drying. Formulations were made using HPLC grade water (CAS 7732-18-5; Fisher Scientific Ottawa, ON, Canada) or deionized water. The ID93 antigen and GLA-SE adjuvant system were formulated separately; manufacturing of these components has been described elsewhere [23].

#### 140 Formulation Composition

Six formulations were assessed as inhalable vaccine candidates. The feedstock composition and the projected material composition of the final dried particles are given in Table 1. Concentrations for several of the main components, including trehalose, GLA-SE, ID93, and Tris buffer, were kept constant for all the formulated liquid feedstocks, as listed in the table.

ID93 protein was stored at a concentration of 1.2 mg/mL at  $-80\text{ }^{\circ}\text{C}$  prior to use. GLA-SE nanoemulsions with a squalene concentration of 10% v/v and GLA concentration of 50  $\mu\text{g/mL}$  were stored in a refrigerator prior to use. All formulation processes began with preparation of 4 mg/ml Tris. The Tris solution was then pH adjusted by addition of hydrochloric acid to a pH of  $7.5\pm 0.1$ . Preliminary work found that the buffer system had no apparent effect on particle morphology. For each formulation, the trehalose and relevant dispersibility enhancing agent were dissolved in water into buffered Tris solution. Once fully dissolved,

GLA-SE was added and the solution gently mixed. ID93 was added last to the feedstock to minimize potential protein binding to container surfaces.

150 Previous work [23] found that a high encapsulation efficiency of the vaccine candidate was achieved by spray drying 4 µg/mL of ID93, 10 µg/mL of GLA, and 17.2 mg/mL of squalene with 100 mg/ml of trehalose. The same ratios of excipient, antigen, and adjuvant system were kept in this work to target a high encapsulation efficiency. The correct antigen and adjuvant concentration for an inhalable route of administration has not been determined and may need to be increased in the future.

**Table 1 Formulation parameters and designed particle composition by mass of the human inhalable vaccine candidates.**

<b>Component\Formulation</b>	<b>T</b>	<b>T20Leu</b>	<b>T10Pul</b>	<b>T20Pul</b>	<b>T3Tri</b>	<b>T6Tri</b>
<b>Feedstock Composition (mg/mL)</b>						
<b>Leucine</b>	-	10.0	-	-	-	-
<b>Pullulan</b>	-	-	4.5	10.5	-	-
<b>Trileucine</b>	-	-	-	-	1.3	2.6
<b>Trehalose</b>	33.3	33.3	33.3	33.3	33.3	33.3
<b>Tris (buffer)</b>	0.807	0.807	0.807	0.807	0.807	0.807
<b>Squalene</b>	5.73	5.73	5.73	5.73	5.73	5.73
<b>DMPC</b>	1.27	1.27	1.27	1.27	1.27	1.27
<b>GLA</b>	0.0033	0.0033	0.0033	0.0033	0.0033	0.0033
<b>ID93</b>	0.0013	0.0013	0.0013	0.0013	0.0013	0.0013
<b>Total Feed Concentration</b>	41.1	51.1	45.6	51.6	42.4	43.7
<b>Particle Composition (w/w)</b>						
<b>Leucine</b>	-	20%	-	-	-	-
<b>Pullulan</b>	-	-	10%	20%	-	-
<b>Trileucine</b>	-	-	-	-	3%	6%
<b>Trehalose</b>	81%	65%	73%	65%	78%	76%
<b>Tris (buffer)</b>	2%	2%	2%	2%	2%	2%
<b>Squalene</b>	14%	11%	12%	11%	14%	13%
<b>DMPC</b>	3%	2%	3%	2%	3%	3%
<b>GLA</b>	0.01%	0.01%	0.01%	0.01%	0.01%	0.01%
<b>ID93</b>	0.003%	0.003%	0.003%	0.003%	0.003%	0.003%

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## 2.2 Spray Drying

Spray drying parameters were chosen in order to minimize potential antigen or agonist losses during processing based on a previous study involving spray drying ID93+GLA-SE [23]. A custom research spray dryer [42] with a twin fluid atomizer was utilized to conduct the spray drying. Use of a twin-fluid atomizer



160 has been reported to significantly reduce degradation of a shear- and temperature-sensitive protein during the atomization step as compared to use of a vibrating mesh atomizer [43, 44]. The atomizer was operated at an air-liquid ratio of 8, corresponding to a mass median initial droplet diameter of approximately 9  $\mu\text{m}$ . Characterization of the atomizer is described elsewhere [45].

A relatively low drying gas temperature of 65  $^{\circ}\text{C}$  was utilized in order to minimize temperature-dependent  
165 degradation. The other spray drying parameters were calculated using an energy and balance model [46] to achieve an outlet humidity of less than 10% relative humidity and low outlet temperature. A low outlet humidity was targeted to achieve a low (2-3%) powder moisture content as over-drying can also lead to protein degradation. A low outlet temperature was chosen to limit the temperature the powder was exposed to during cyclone collection. The feedstock was supplied to the atomizer at a rate of 0.6 mL/min using a  
170 peristaltic pump (Model 77200-60; Cole-Parmer, Montreal, QC, Canada), and the drying gas flow rate was set to 200 SLPM, leading to a low outlet temperature of approximately 36  $^{\circ}\text{C}$ . Powders were stored under dry conditions prior to characterization.

## 2.3 Particle Design

### Respirable Range

175 The target particle aerodynamic diameter range for this study was chosen to be 3-4  $\mu\text{m}$ . The range in feedstock concentration to produce particles within the target size range was calculated using Eq. 1, where,  $d_a$ , is the aerodynamic diameter,  $\rho_p$  is the particle density,  $\rho^*$  is the reference density (1000  $\text{kg}/\text{m}^3$ ),  $c_F$  is the feedstock concentration, and  $d_D$  is the diameter of the droplets [38]. Further details on the derivation of this equation can be found elsewhere [38].

$$d_a = \sqrt[6]{\frac{\rho_p}{\rho^*}} \sqrt[3]{\frac{c_F}{\rho^*}} d_D \quad 1$$

180

Previous work has shown that spray drying the ID93+GLA-SE vaccine produces particles with varying shell thicknesses [23]. Material density of this formulation was estimated to be 1438  $\text{kg}/\text{m}^3$ . Previous studies

on spray drying of emulsions [47, 48] and spray drying formulations containing leucine [34] have shown that the resulting particles are hollow, with varying degrees of shell thicknesses. Spray drying of formulations containing trileucine have been shown to produce particles with external void space [39]. Based on these findings, preliminary calculations assumed that the average particle in this study contained approximately 30% void space. Therefore, the particle density can be roughly approximated to be 1000 kg/m<sup>3</sup>. Initial droplet diameter was predicted to be 9 μm based on the processing conditions. Based on these assumptions, the concentration of the feedstock must be between 37 and 88 mg/mL to achieve a particle size between 3 and 4 μm.

### **Selection of Excipients to Improve Powder Dispersibility**

Aerodynamic particle size is a strong indicator of a powder's ability to deposit within the lung. Therefore, dispersing particle aggregates into primary particles is essential; otherwise, aggregated small particles will behave aerodynamically as larger particles and potentially deposit prior to the lung. However, passive delivery devices, such as DPIs, can only provide limited dispersing force as they rely solely on the patients' inhalation flow to de-aggregate the loaded powder dosages. Thus, it is necessary to reduce intrinsic powder cohesiveness to improve the dispersibility. Powder cohesiveness can be described in terms of the contact mechanics between adjacent particles. Based on theoretical cohesion models, e.g. the Li-DMT model [49], the force of cohesion between two particles,  $F_c$ , can be reduced by lowering the surface energy, decreasing the deformability of the surface, and decreasing the contact area.

The excipients investigated in this study, leucine, pullulan, and trileucine, were expected to reduce the force of cohesion between particles. The component mass fraction for all investigated dispersibility enhancing agents in this study was limited to a maximum of 20% in order to maximize the adjuvant dose in the powder. Leucine was chosen as it has been reported to change the surface morphology of spray-dried particles through formation of a crystalline surface layer. Increasing leucine concentration changes particle surface from a smooth morphology to solid particles with corrugated surfaces [34, 35]. Additional increases in leucine concentration further changes particle morphology to rugose hollow particles. The increased surface

roughness due to crystal surface asperities is expected to reduce effective contact area between particles. Additionally, the formation of a crystalline outer layer is expected to reduce the deformability of the surface as compared to an amorphous particle surface. Feng et al. [34] reported that, for their given spray drying parameters, 25% leucine mass fraction in a leucine-trehalose system was required to achieve complete crystallinity of leucine. Thus, a mass fraction of 20% leucine was chosen for the T20Leu formulation to promote crystal growth in order to improve powder dispersibility.

Pullulan was chosen as it has been shown to introduce particle folding in pullulan-trehalose systems [37]. The change in surface morphology may decrease effective contact area, depending on particle orientation. Carrigy et al. [37] reported that the formation of folded, irregularly shaped particles increases with increasing pullulan concentration, and 10% pullulan mass fraction in a pullulan-trehalose system slightly improved aerosol performance as compared to a trehalose-only formulation. Based on these results, a mass fraction of 10% pullulan was chosen for the T10Pul formulation in order to modify the surface morphology to promote improved dispersibility. Due to the reported increase in particle folding with increased pullulan content, a mass fraction of 20% pullulan for the T20Pul formulation was also investigated.

Trileucine was chosen as it has been reported to form highly wrinkled particle surfaces with increasing concentration, and has been shown to decrease the surface energy of spray-dried particles [39, 40]. Highly rugose particle surface morphologies are expected to decrease contact area between particles, and reduced surface energy is expected to reduce the force of cohesion between particles. Wang et al. [40] demonstrated that at 1.0% mass fraction of trileucine in trileucine-trehalose systems the particle morphology appears rugose. Particle surface rugosity was improved greatly when the trileucine mass fraction was increased to 5.0%. Due to trileucine solubility limitations, 6% trileucine by mass for the T6Tri formulation was chosen for investigation in this study. 6%, a relatively high mass fraction, was chosen in order to promote increased particle surface rugosity and thus reduce particle cohesion. A lower mass fraction of 3% for the T3Tri formulation was also investigated in this study to determine if a similar performance could be obtained with a formulation with lower excipient costs.

## Particle Formation Model

Previous studies have reported the mass fractions of leucine, pullulan, and trileucine required to induce surface morphology changes. However, these studies utilized different spray drying processing conditions. Change in processing conditions will affect the distribution of components within a drying droplet. A simple particle formation model [50] was used to predict drying time and component distribution of the investigated formulations to verify that the dispersibility agents will form a shell on the particle exterior for the given spray drying parameters.

As the droplet dries, the radial concentration gradient of the formulation components is controlled by two mechanisms: the receding droplet surface and the diffusion of solutes from the surface towards the center of the droplet [50, 51]. The former mechanism will increase surface concentration whereas the latter will decrease surface concentration. This relationship can be described by the dimensionless Péclet number,  $Pe$ . The Péclet number is the ratio of the evaporation rate,  $\kappa$ , and the diffusion coefficient,  $D$ , of a component  $i$ , as seen in Eq. 2. For a  $Pe$  close to 1 or smaller, the material will be able to diffuse quickly relative to receding droplet surface and thus will be evenly distributed. For a large  $Pe$ , the component is expected to be relatively immobile and therefore accumulate near the droplet surface.

$$Pe_i = \frac{\kappa}{8D_i} \quad 2$$

$Pe$  can be used to determine the surface enrichment of a given component. Surface enrichment is the surface concentration of a component,  $c_{s,i}$ , relative to its mean concentration within the droplet,  $c_{m,i}$ . Surface enrichment for a component with a  $Pe$  smaller than 20 can be approximated using Eq. 3 [38], in which the steady state surface enrichment value,  $E_{ss}$ , assumes that the solute concentration within the droplet changes at the same rate as the mean concentration.

$$E_{ss} = \frac{c_{s,i}}{c_{m,i}} \approx 1 + \frac{Pe_i}{5} + \frac{Pe_i^2}{100} - \frac{Pe_i^3}{4000} \quad 3$$

Steady state surface enrichment for  $Pe$  values larger than 20 can be approximated using Eq. 4 [50]. Further discussion on  $Pe$  and surface enrichment can be found elsewhere [50].

$$E_{ss} \approx \frac{Pe_i}{3} + 0.363 \quad 4$$

255  $E_{ss}$  was used to approximate the time when a particle shell will form. The time at which shell formation is expected to start for components that do not crystallize is the time it takes a component to reach a concentration at the surface equivalent to its true density,  $\tau_{t,i}$ . The time at which shell formation is expected to start for components that do crystallize is the time that the component reaches critical supersaturation at the surface,  $\tau_{s,i}$ . The  $\tau_{t,i}$ , is given in Eq. 5, where  $C_{0,i}$  is the initial concentration of component  $i$  and  $\rho_{t,i}$  stands for its material true density, and  $\tau_D$  is the droplet drying time. As the formulations investigated contain multiple components, true density of a mixture,  $\rho_{t,mix}$ , was calculated and substituted for  $\rho_{t,i}$ . The calculation of  $\rho_{t,mix}$  is described elsewhere [37]. The  $\tau_{s,i}$  is given in Eq. 6, where  $C_{sol,i}$  is the solubility of component  $i$ .

$$\tau_{t,i} = \tau_D \left[ 1 - \left( \frac{C_{0,i}}{\rho_{t,i}} E_i \right)^{\frac{2}{3}} \right] \quad 5$$

$$\tau_{s,i} = \tau_D \left[ 1 - \left( \frac{C_{0,i}}{C_{sol,i}} E_i \right)^{\frac{2}{3}} \right] \quad 6$$

265 The evaporation rate of a pure water droplet at the drying gas temperature, 65 °C, is  $3.7 \times 10^{-9}$  m<sup>2</sup>/s [51]. The diffusion coefficient of pullulan was approximated to be  $2.8 \times 10^{-11}$  m<sup>2</sup>/s [37]. The diffusion coefficient for trehalose in water,  $D_{tre}$ , was calculated to be  $3 \times 10^{-10}$  m<sup>2</sup>/s using Eq. 7 [52], where  $w_s$  is the mass fraction of solute and  $T$  is droplet temperature in K, i.e. 301 K [23]. This equation was obtained by fitting an equation to experimental data of trehalose diffusion in aqueous solutions [53].

$$D_{\text{tre}} = \frac{5 \times 10^{-8}}{e^{-13(w_s)^{1.1}}} e^{-1500 \frac{e^{1.9 w_s}}{T}} \quad 7$$

270 Diffusion coefficients for other solutes were approximated based on molecular size using the Einstein-Stokes equation. The GLA-SE nanoemulsion droplets were considered as a component for the sake of diffusion calculations. The diffusion coefficient of the nanoemulsion droplets has been previously approximated to be  $5.3 \times 10^{-12}$  m<sup>2</sup>/s using the Einstein-Stokes equation, assuming that the nanoemulsion droplets remain stable as an aqueous dispersion and can be treated as nanoparticles [23].

275 The size of a peptide was approximated based on its mass using Eq. 8, assuming the peptide is in the shape of a sphere [54]. Eq. 8 determines  $R_{\text{min}}$  of a peptide, the minimum radius of a sphere that could contain its mass.  $R_{\text{min}}$  is given in nm and  $M$  is the molecular weight of the peptide, given in Da. Based on this equation, the diffusion coefficient for leucine was approximated to be  $6.3 \times 10^{-10}$  m<sup>2</sup>/s and the diffusion coefficient for trileucine was approximated to be  $4.5 \times 10^{-10}$  m<sup>2</sup>/s.

$$R_{\text{min}} = 0.066M^{1/3} \quad 8$$

280 Distribution calculations for ID93 were not conducted as previous work has reported that an estimated 96% of the antigen is associated with the adjuvant [55]. The literature values for the density and solubility of the given components are summarized in Table 2. Table 2 also shows the calculated  $Pe$  and  $E_{ss}$  for each component.

285 **Table 2 Density and solubility values from literature, and calculated  $Pe$  and  $E_{ss}$  for the main components of the spray-dried inhalable vaccine candidates.**

Component	Density (kg/m <sup>3</sup> )	Solubility (mg/mL)	$Pe_i$	$E_{ss,i}$	References
Trehalose	1580	690	1.4	1.3	[40], [52]
Leucine	1293	23	0.7	1.1	[56]
Pullulan	1850	Variable	17	6.1	[57], [58]
Trileucine	1250	6.8	1	1.2	[41], [39]
GLA-SE	N/A	N/A	90	30	

Non-crystallizing components with a  $Pe$  near 1 and high solubility, such as trehalose, are expected to form solid particles later in the droplet lifetime with even component distribution. The  $Pe$  of both pullulan and

the GLA-SE emulsion droplets was much greater than 1, suggesting that these components will accumulate  
290 near the surface of the drying droplet. Previously, encapsulation of the vaccine candidate with trehalose via  
spray drying showed that the GLA-SE droplets are distributed throughout the trehalose matrix, with  
increasing radial concentration towards the particle surface [23].

A summary of the calculated particle formation parameters is given in Table 3, with calculations based on  
the values given in Table 2. These simplified calculations assume a constant  $Pe$  to provide an estimated  
295 timeline of the drying processes without looking into the detailed droplet drying steps. For example,  
formation of crystals will increase the  $Pe$  due to increasing component size, which will further facilitate  
surface enrichment. Similarly, increasing viscosity near the droplet surface due to increasing solute  
concentration over time will increase the  $Pe$  and thus facilitate shell formation. This particle formation  
model also neglects the effect of surface activity. Inclusion of these considerations results in very complex  
300 models that are outside the scope of this study.

Time to true density was calculated for trehalose and pullulan as neither are crystallizing systems under  
normal spray drying conditions. For trileucine, the phase separation is not fully understood at this time,  
however, previous studies have shown that it forms a shell soon after reaching saturation [1, 41, 40]. For  
this reason, the time to saturation was calculated for trileucine.

305 It is apparent that the trehalose will reach the true density of the given mixture relatively late (>90%) in the  
droplet lifetime for all formulations. The calculations predict that leucine reaches critical saturation  
relatively early (37.2%) in the droplet lifetime and therefore forms an outer shell composed of growing  
crystals. Pullulan was predicted to reach true density close to the same time as trehalose (93.0% and 87.9%),  
which suggests that the outer surface of these particles may be composed of both pullulan and trehalose.

310 The model predicts that trileucine will accumulate on the surface and form a shell early in the drying process  
due to relatively short time to reach saturation (62.3% and 40.2%). Therefore, the model predicts that the  
chosen mass fractions are likely to result in partial to total particle surface coverage with the dispersibility  
enhancing agents for the chosen spray drying parameters.

315 **Table 3 Feed concentrations of each component, true density, and normalized time for each component to reach true density or saturation for each inhalable vaccine formulation. Abbreviations: tre – trehalose, leu – leucine, pull – pullulan, tri – trileucine.**

Formulation	$C_{0,tre}$ (mg/mL)	$C_{0,leu}$ (mg/mL)	$C_{0,pull}$ (mg/mL)	$C_{0,tri}$ (mg/mL)	$\rho_{t,mix}$ (kg/m <sup>3</sup> )	$\frac{\tau_{t,tre}}{\tau_D}$	$\frac{\tau_{s,leu}}{\tau_D}$	$\frac{\tau_{t,pull}}{\tau_D}$	$\frac{\tau_{s,tri}}{\tau_D}$
T	33.3	-	-	-	1438	90.3%	-	-	-
T20Leu	33.3	10	-	-	1411	90.2%	37.2%	-	-
T10Pul	33.3	-	4.5	-	1473	90.5%	-	93.0%	-
T20Pul	33.3	-	10.5	-	1510	90.6%	-	87.9%	-
T3Tri	33.3	-	-	1.3	1428	90.3%	-	-	62.3%
T6Tri	33.3	-	-	2.6	1425	90.3%	-	-	40.2%

## 2.4 Dry Powder Characterization

Field Emission Scanning Electron Microscopy (Zeiss Sigma FE-SEM; Carl Zeiss, Oberkochen, Germany) was used to determine particle morphology for the inhalable vaccine candidates. Powder samples were mounted either directly onto aluminum SEM stubs (Product 16111; Ted Pella, Inc.; Redding, CA, USA) or onto carbon tape placed over the stubs. The former method included scraping the powder against the stubs in order to intentionally crack particles open to view the interior structure. The latter method was implemented to avoid intentional destruction of the particles in order to view the exterior structure. These samples were placed in a desiccator connected to an in-house vacuum system for 1-4 days to remove the exposed nanoemulsion droplets and prevent damage to the electron microscope. Following desiccation, the samples were sputtered with a coating of 80% gold and 20% palladium (Leica ACE600 Carbon/Metal Coater; Concord, ON, Canada) to a thickness of 10-15 nm or with a coating of gold (Denton Vacuum Desk II Sputter Coater; Denton, Moorestown, NJ, USA) to a thickness of approximately 16 nm. Images ranging from magnifications of 500 to 25000 $\times$  were taken at a working distance of 5.4-6.8 mm using an accelerating voltage of 4-5 kV.

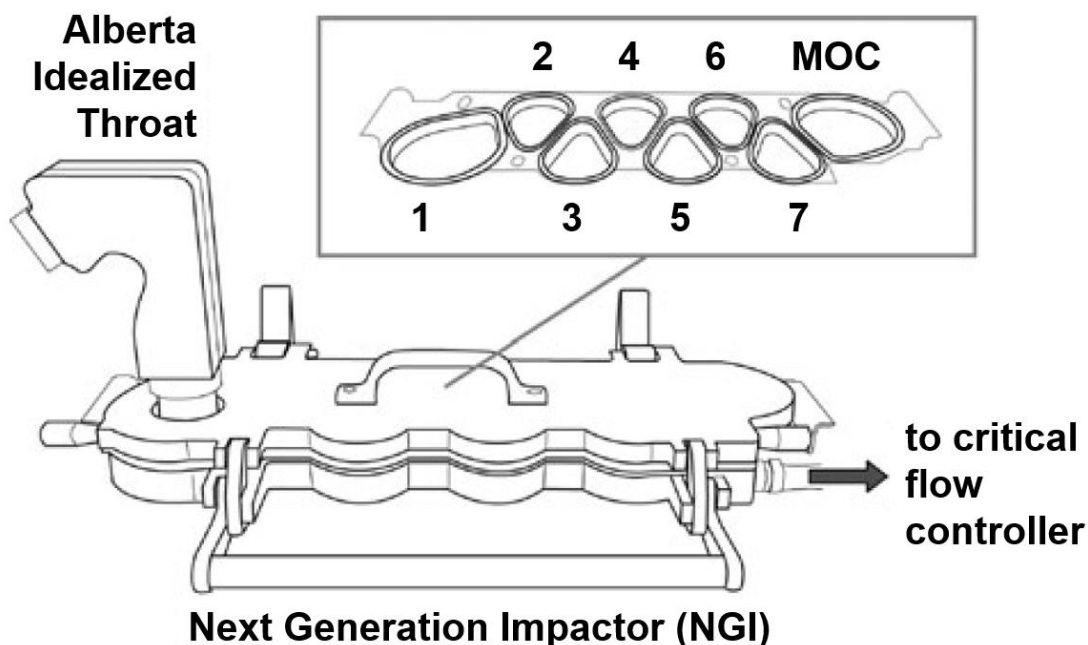
The solid phase of the powder was assessed by Raman spectroscopy to determine powder crystallinity for each spray-dried formulation using a custom dispersive Raman spectroscopy system. A detailed description of a similar apparatus has been published elsewhere [59]. All spectra were measured at a temperature of 22.0-23.0 °C and at less than 3% RH to prevent moisture exposure. Raman spectrum analysis was also



conducted on crystalline trehalose, crystalline leucine, raw crystalline trileucine, crystalline Tris, and raw pullulan as references. Neat trehalose and neat trileucine from aqueous formulations were spray-dried with a bench top spray dryer under similar spray-drying conditions used in this study. These spray-dried trehalose and spray-dried trileucine powders were analyzed as amorphous references.

340 Reference spectra were also obtained for a liquid sample of squalene. The amorphous leucine spectrum was obtained by subtracting the water spectrum from a concentrated aqueous leucine solution (20 mg/mL) spectrum. It has been previously demonstrated that spectra of amorphous solids are similar to a concentrated aqueous solution of the solid [60].

Lung deposition was measured *in vitro* using a Next Generation Impactor (NGI) (Copley Scientific; 345 Nottingham, UK) with an Alberta Idealized Throat (AIT) attachment. The AIT mimics the general geometry of a human mouth-throat [61]. Grgic et al. [62] established that particle deposition using the model is in agreement with human experimental extrathoracic deposition data. A simplified schematic of this set up is shown in Figure 1.



**Figure 1** *In vitro* aerosol performance testing apparatus [45]. The Alberta Idealized Throat was utilized to obtain a reasonable approximation of vaccine powder deposition in the human oral cavity and pharynx (mouth-throat) region.

**The Next Generation Impactor consists of seven stages and a micro-orifice collector (MOC) for assessment of particle size distribution.**

350 A commercial low resistance DPI (Seebri Breezhaler, Novartis International AG; Basel, Switzerland) was used to deliver the powder. The DPI has been characterized elsewhere [63]. The DPI was connected to the throat model using a custom 3D-printed mouthpiece adapter. A similar set up was used in Hoe et al. [45] and Carrigy et al. [37]. Inhalation flow rate was simulated via a critical flow controller (Critical Flow Controller Model TPK 2000, Copley Scientific Limited; Nottingham, UK) connected to a vacuum pump  
355 (Maxima M16C, Fisher Scientific; Ottawa, ON, Canada). This set up was utilized to obtain an assessment of loss due to extrathoracic powder deposition under normal use. A similar procedure was followed as given in Carrigy et al. [37]. Prior to the experiment, the impactor stages, the micro-orifice collector (MOC) and the interior of the throat model were coated with silicone spray (Molykote 316 Silicone Release Spray, Dow Corning Corporation; Midland, MI, USA) to mitigate particle bounce [64]. Powder was manually loaded  
360 into size 3 hydroxypropyl methylcellulose capsules (Quali-V-1; Qualicaps, Inc., Madrid, Spain) in a dry glovebox. Each capsule contained  $41 \pm 9$  mg of powder. Actuation and inhalation was performed using three capsules in succession to obtain sufficient mass on the impactor stages and MOC for gravimetric analysis. Inhalation was simulated at an inspiratory flow rate of 100 L/min over 2.4 seconds to achieve 4 L of air withdrawal as per the USP 601 monograph [65]. Experiments were performed in triplicate and  
365 conducted under ambient conditions. A two-tailed student's t-test was used for analysis, where statistically significant differences were reported for  $p < 0.05$ .

All gravimetric measurements were conducted with a microbalance (ME204E, Mettler Toledo; Mississauga, ON, Canada). Capsules were weighed before and after powder loading to determine the mass of powder added. The DPI containing the loaded capsule was measured before and after actuation to  
370 determine the emitted dose, defined as the percentage of loaded mass that exited the inhaler. Lung dose was defined as the percentage of loaded mass that penetrated the throat model. Lung dose was calculated as the total powder deposition on the impactor stages relative to the loaded powder mass. Powder deposition was

determined gravimetrically by measuring the stages before and after the experiment run. Correlation of mass distribution to particle size was based on stage cutoff diameters at 100 L/min flow rate, as determined elsewhere [66].

Mass median aerodynamic diameter,  $d_{a,50}$ , and geometric standard deviation,  $\sigma_g$ , of the deposited powder was calculated by fitting the data to a cumulative lognormal distribution function [37]. In this case,  $d_{a,50}$  and  $\sigma_g$  measured are for the powder that has deposited within the impactor, not the size distribution of the spray-dried formulations themselves. Real-time sampling during production to obtain the  $d_{a,50}$  and  $\sigma_g$  of the spray-dried formulations could not be completed due to equipment issues. Data fitting was done using the MATLAB (MathWorks Inc., Natick, MA, USA) “Curve Fitting” application. For a given stage, the cutoff diameter was plotted as the upper size limit for each bin, and the deposition fraction for each bin was calculated with respect to the total amount of powder deposited on the stages.

As previously indicated, inhalable aerosols can be administered through the intranasal or pulmonary route. The spray-dried powders investigated in this study were designed for delivery to the lungs through inhalation past the mouth. Powders designed for intranasal delivery through the nose would have to be assessed for deposition through other methods; however, this model can be used to provide an indication of powder dispersibility for a given formulation.

## 2.5 Reconstituted Powder Characterization

All samples were reconstituted to the feedstock concentrations with freshly dispensed MilliQ water for analysis. Nanoemulsion droplet diameter, polydispersity index, squalene concentration, GLA concentration, and ID93 presence were evaluated in the reconstituted powders. Similar experimental techniques were used previously to assess retention of vaccine components in spray-dried powder [23].

Mean hydrodynamic diameter and polydispersity of the nanoemulsion droplets in liquid formulations were measured using a dynamic light scattering technique (Zetasizer APS; Malvern, Worcestershire, UK). Polydispersity index was calculated as the standard deviation of the measured size distribution divided by

the mean hydrodynamic diameter, squared. Details of the measurement process have been described elsewhere [67]. Reported average and standard deviation measurements for each sample are from the same sample analyzed 3 times.

400 Squalene content was quantified using a reverse phase HPLC method. Separation of squalene from sample was performed on an Agilent 1200 HPLC (1200 HPLC; Agilent Technologies; Santa Clara, CA, USA) equipped with a silica-based, C18 reversed-phase column (Atlantis T3 Column; Waters; Elstree, UK). Column temperature was held constant at 30 °C and analyte detection was accomplished using a charged aerosol detector (Corona CAD; ESA Biosciences; Chelmsford, MA, USA). Mobile phase A contained  
405 75:15:10 (v/v/v) methanol:chloroform:water, 1% (v/v) acetic acid, and 20 mM ammonium acetate and mobile phase B contained 50:50 (v/v) methanol:chloroform, 1% (v/v) acetic acid, and 20 mM ammonium acetate. Samples were diluted in mobile phase B and injected with a gradient over 30 minutes. Squalene content was quantitated by peak area. Concentration measurements were made by interpolation of a curve generated from standards fitted with a second order polynomial. Reported average and standard deviation  
410 measurements for each formulation are from two separately prepared HPLC samples.

GLA content was also quantified using a reverse phase HPLC method, in which separation of GLA from sample was done with the same equipment and the same mobile phases. Samples were diluted in mobile phase B and injected with a gradient over 18 minutes. Column temperature was held constant at 30 °C. GLA content was quantitated by peak height. Concentration measurements were made by interpolation of  
415 a curve generated from standards fitted with a second order polynomial. Reported average and standard deviation measurements for each formulation are from two separately prepared HPLC samples.

Due to insolubility in the HPLC buffers, samples that contained pullulan were diluted with the appropriate volume of mobile phase B, capped, and then centrifuged on an EZ-2 Mk2 centrifugal evaporator (Genevac LTD, Ipswich, England) for 20 minutes on the low boiling point setting with a maximum temperature set  
420 to 35°C. A 200 uL aliquot of sample was transferred to a new HPLC vial and then injected as normal. An

internal standard containing either GLA or squalene was included to ensure no analyte loss upon centrifugation or transfer. Care was used not to disturb the pullulan pellet upon transfer.

The presence of ID93 in formulated samples was determined using SDS-PAGE. Gel samples were prepared by mixing 4X LDS Buffer (Thermo Fisher Scientific, Waltham, MA, USA) spiked with 5% (v/v)  $\beta$ -Mercaptoethanol, a 20% (w/v) sodium dodecyl sulfate solution (Thermo Fisher Scientific, Waltham MA, USA), and formulated sample in a 1:2:1 ratio. Prepared samples were heated in an 85°C water bath for 15 minutes, and then left to cool in a room temperature water bath. A precast, 4-20% Tris-Glycine SDS-PAGE gel (Thermo Fisher Scientific, Waltham, MA, USA) was prepared according to manufacturer's instructions for denaturing gel electrophoresis using Tris-Glycine SDS Running Buffer (Thermo Fisher Scientific, Waltham, MA, USA) and the recommended gel tank and power supply (Thermo Fisher Scientific, Waltham, MA, USA). Cooled gel samples were centrifuged at 2000 RPM in a benchtop centrifuge (Thermo Fisher Scientific, Waltham, MA, USA) for 2 minutes to collect the sample, and then briefly vortexed prior to loading onto the prepared gel. Mark12 ladder (data not shown) (Thermo Fisher Scientific, Waltham, MA, USA) was diluted 1:4 with freshly dispensed MilliQ water and also run on the gel as a molecular weight marker to confirm the expected migration of ID93 through the gel. The gel was run at 180V for 65 minutes, and then stained overnight using Sypro Ruby stain (Thermo Fisher Scientific, Waltham, MA, USA) according to the manufacturer's instructions. Stained gels were imaged using a gel imaging system (ChemiDoc; Bio-Rad, Mississauga, ON, Canada) employing the manufacturer's settings for Sypro Ruby stain. Duplicate gels were run to confirm the presence or absence of the ID93 monomer band.

## 440 **3 Results and Discussion**

### **3.1 Particle Morphology**

The particles for a given formulation exhibited consistent morphology. Representative SEM images of the inhalable vaccine candidates are shown in Figure 2. The spray-dried T formulation particles visually appear to be within respirable range. The particles' surface ranges from smooth to slightly dimpled, which was

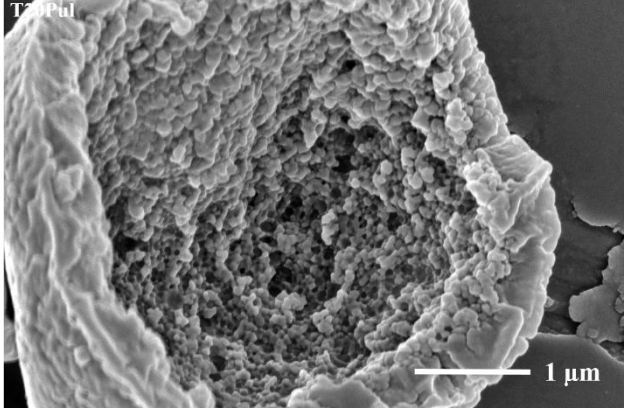
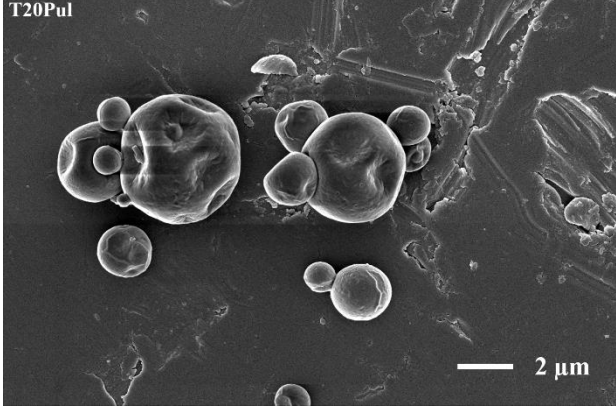
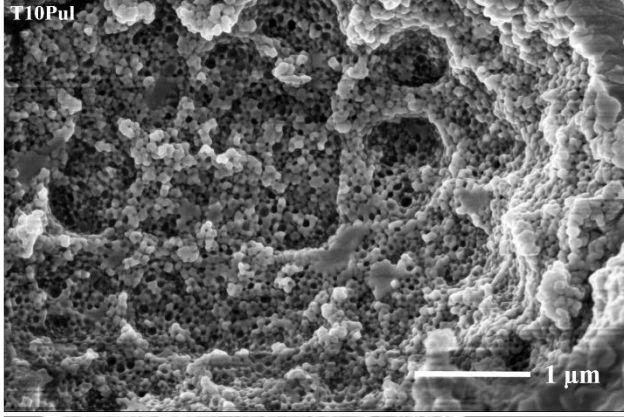
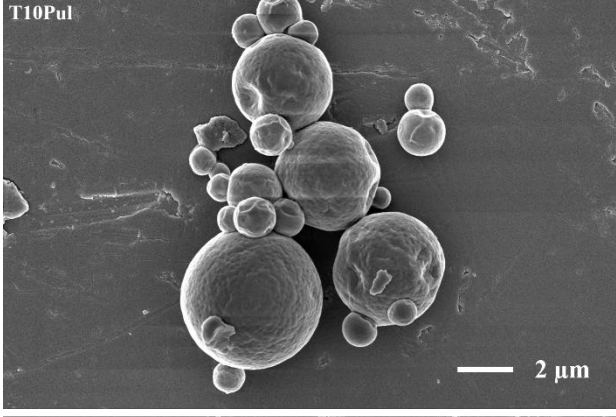
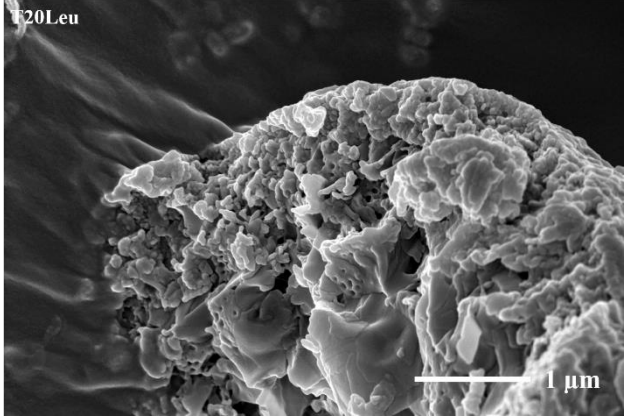
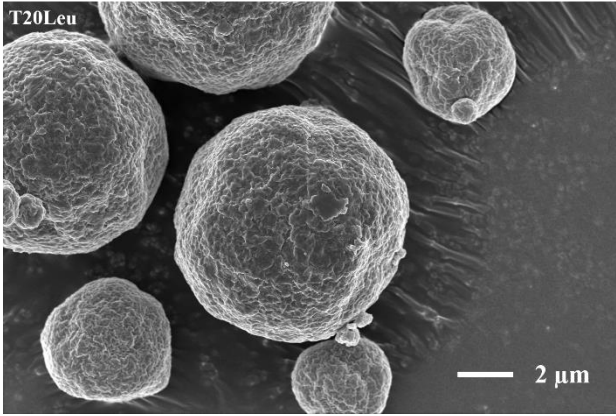
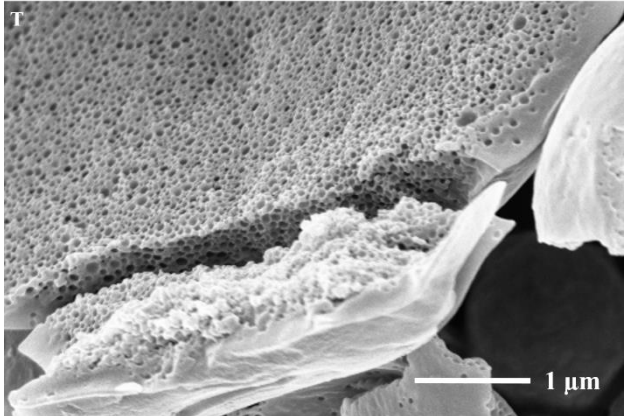
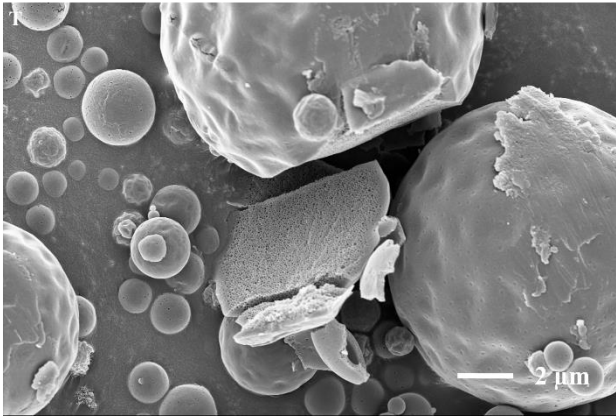
445 consistent with previous studies on spray drying ID93+GLA-SE vaccine with trehalose [23] and spray-  
dried bacteriophages encapsulated in trehalose [41, 68]. The smooth disaccharide particle surface is  
undesirable in terms of powder dispersibility as smooth surfaces are more cohesive than rugose surfaces.  
Interior analysis of cracked particles revealed the presence of many small voids. These voids are caused by  
the encapsulated nanoemulsion droplets within the amorphous trehalose matrix. Particle interiors feature  
450 either a large central void or many central voids (not shown) and exhibit a range of shell thicknesses, which  
was consistent with previous work [23].

Like the T formulation, the spray-dried T20Leu particles also appear to be within respirable range. Unlike  
the T formulation, T20Leu particle surfaces were rough, with many surface asperities. These surface  
asperities are likely individual leucine crystals. Similar surface morphology has been produced in spray-  
455 dried crystalline leucine and trehalose systems [34, 41]. The presence of leucine crystals at the particle  
surface was also predicted by the particle formation model; the formulation was designed such that leucine  
reached saturation on the surface early in the droplet evaporation process, providing the necessary time to  
form a shell on the surface before trehalose. Analysis of the cracked particle suggests that the T20Leu  
particles are composed of a trehalose core that transitioned into a crystalline leucine surface layer. Like the  
460 T particles, the nanoemulsion droplets are encapsulated within the spray-dried T20Leu particles.

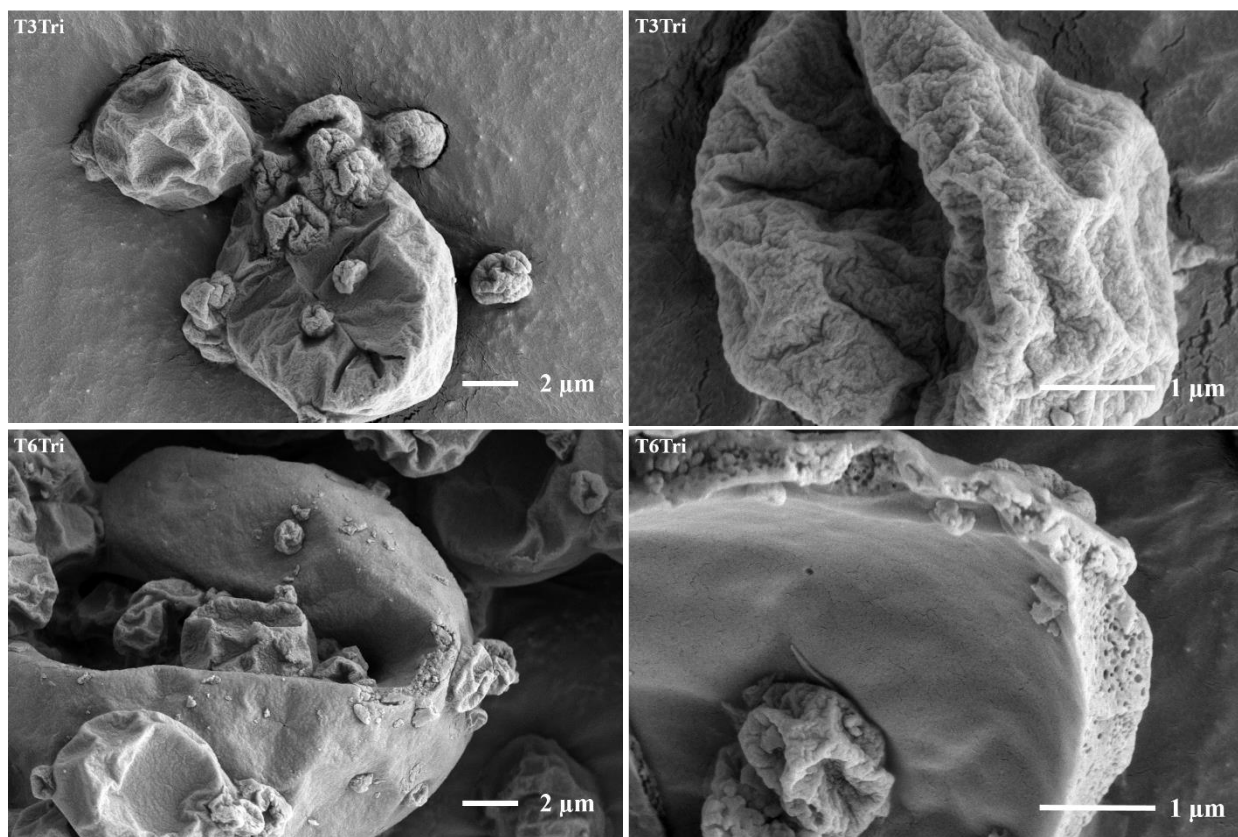
Both the pullulan-containing formulations, T10Pul and T20Pul, produced dimpled particles which appear  
to be within respirable range. Increased number and depth of dimples was shown with increasing pullulan  
concentration. The surface particle morphology and increasing dimpling shown with increasing pullulan  
content were consistent with studies involving spray drying of trehalose-pullulan systems [37]. The dimpled  
465 morphology was not seen in the T particles, suggesting that the particle formation model correctly predicted  
that pullulan would enrich the surface. Interior particle morphology showed that the nanoemulsion droplets  
are encapsulated within the particle wall for both the pullulan containing formulations. Cracked particles  
appeared to be hollow, with a range of shell thicknesses (not shown). Unlike the T20Leu formulation, it  
was difficult to visually determine the presence or location of a radial pullulan-trehalose transition. Lack of

470 clear transitional layer was expected as trehalose and pullulan are amorphous materials with no discernable visual difference at the given magnification.

The spray-dried formulations containing trileucine, T3Tri and T6Tri, produced highly folded particle surfaces, with increased wrinkles exhibited with increased trileucine concentration. Exterior particle morphology was consistent with previous work on spray-dried trileucine-trehalose systems, which  
475 produced particles with low particle density, i.e. containing interior or exterior void space, or both [41, 40]. Increased corrugation of particles with increasing trileucine concentration had also been demonstrated in other systems [39]. The trileucine layer at the surface of the particles was predicted by the particle formation model as the time for trileucine saturation preceded time for trehalose precipitation. Folded surface morphology was due to the formation of a trileucine shell early in the particle formation process [40]. The  
480 particles collapsed due to the lack of early shell mechanical strength during the drying process and thus appear rugose. Increased trileucine concentration led to earlier shell formation; thus, the formulation with higher trileucine content showed particles with increased levels of folding. The T6Tri formulation's cracked particle image indicated that the nanoemulsion droplets were encapsulated within the particle. A cracked particle could not be found for the T3Tri formulation; however, the interior morphology was expected to  
485 be similar to T6Tri interior morphology due to formulation similarity.





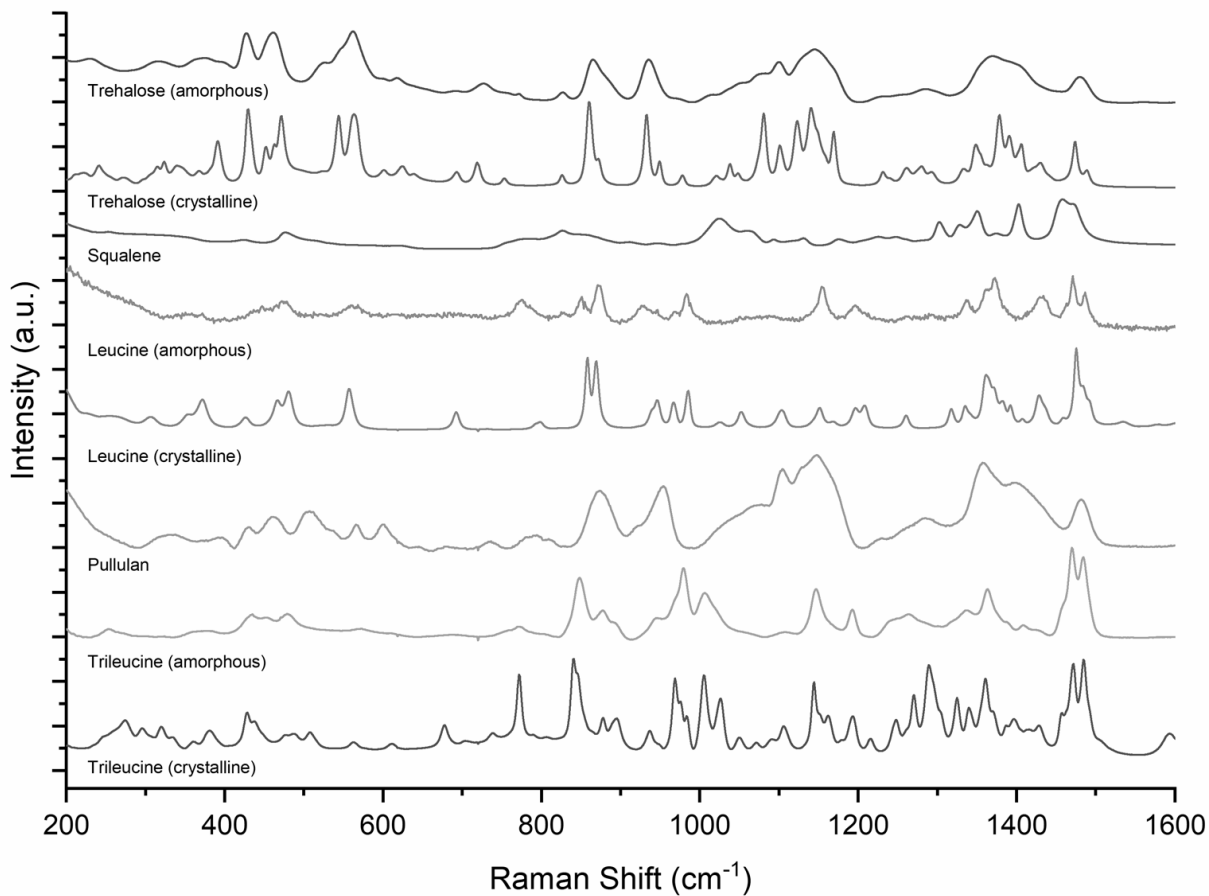


**Figure 2** Low (left) and high (right) magnification SEM images of the inhalable vaccine candidates T, T20Leu, T10Pul, T20Pul, T3Tri, and T6Tri from top to bottom. SEM images showed that exterior particle morphologies vary based on excipient combination. Images of cracked particles indicate the encapsulation of vaccine nanoemulsion droplets. Scale bars are shown on respective images.

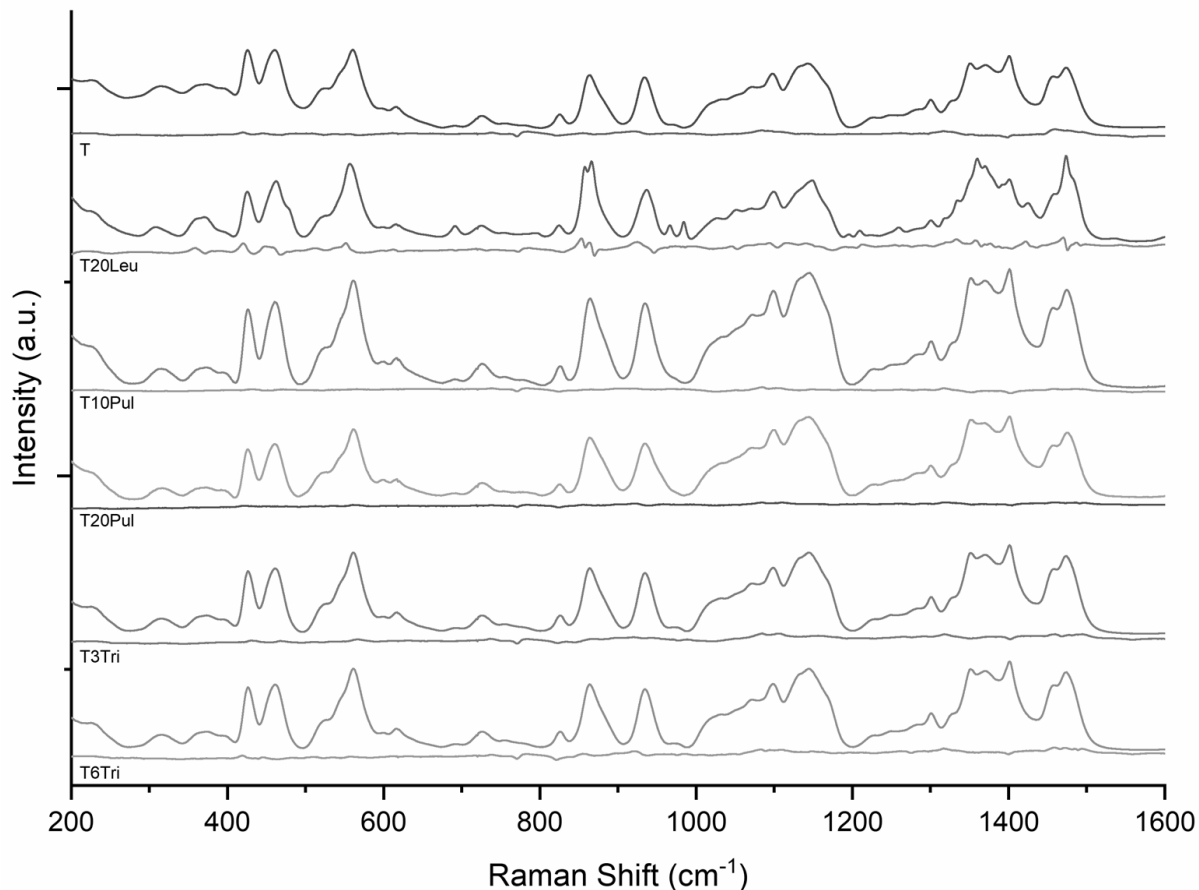
### 3.2 Crystallinity Analysis

The Raman spectra of the inhalable vaccine candidates were analyzed to determine the solid phase of the spray-dried powder. The reference spectra for amorphous and crystalline trehalose, squalene, amorphous and crystalline leucine, pullulan, and amorphous and crystalline trileucine are shown in Figure 3. The ID93 and GLA contributions were not considered due to their low mass fraction. The Raman spectra for the inhalable vaccine candidates are shown in Figure 4. The residual spectrum after partial deconvolution is given under the respective formulation. Partial deconvolution was completed by subtracting the amorphous trehalose, squalene, and Tris reference spectra for all inhalable candidates. Additionally, for the formulations with dispersibility enhancing agents, crystalline leucine, pullulan, and amorphous trileucine

reference spectra were subtracted from the T20Leu, T10Pul and T20Pul, and T3Tri and T6Tri formulations, respectively. Details on the deconvolution process are discussed elsewhere [60].



**Figure 3** Reference spectra for the main components of the inhalable vaccine candidates: trehalose, squalene, leucine, pullulan, and trileucine. Amorphous and crystalline reference spectra are shown where applicable.



**Figure 4** Raman spectra of spray-dried inhalable vaccine candidates. Respective residual spectra are given underneath the given inhalable candidate sample spectra. Primarily amorphous structure is shown in all candidates, as indicated by the relatively low intensity residual spectra. The leucine-containing T20Leu formulation was the only spectrum that exhibited some crystalline peaks. Peaks shown in the residual spectrum for the T20Leu formulation suggest that the leucine component was mostly crystalline.

Deconvolution indicated that the trehalose component of all formulations was completely amorphous, as expected. The amorphous trehalose spectrum dominated the sample spectra as trehalose was the most abundant component in all formulations, with a designed mass fraction of 65-81%. All spray-dried vaccine powders, except for the T20Leu formulation, exhibit fully amorphous spectra, as indicated by the relatively low intensity residual spectra. The T20Leu spectrum features several crystalline leucine peaks, most noticeably at 966 and 984  $\text{cm}^{-1}$ . The T20Leu formulation was designed to have a crystalline outer leucine layer, whereas all other formulations utilized dispersibility enhancing agents that were predicted to form an amorphous shell. These results provide additional evidence that the surface asperities shown in T20Leu morphology analysis are leucine crystals. Further spectral deconvolution indicated the presence of leucine

510 in its amorphous state, which is consistent with the findings of other studies [34]. This study considered formulations with dispersibility enhancing agents  $\leq 20\%$  by mass fraction in order to maximize the adjuvant dose in the powder. However, Feng et al. [34] previously established that a critical crystallization time for the given system must be surpassed in order for the leucine component to be completely crystalline. Leucine crystallinity can be improved by increasing the crystallization time, for example by either increasing the  
515 mass fraction or feed concentration.

### 3.3 Nanoemulsion Size Distribution

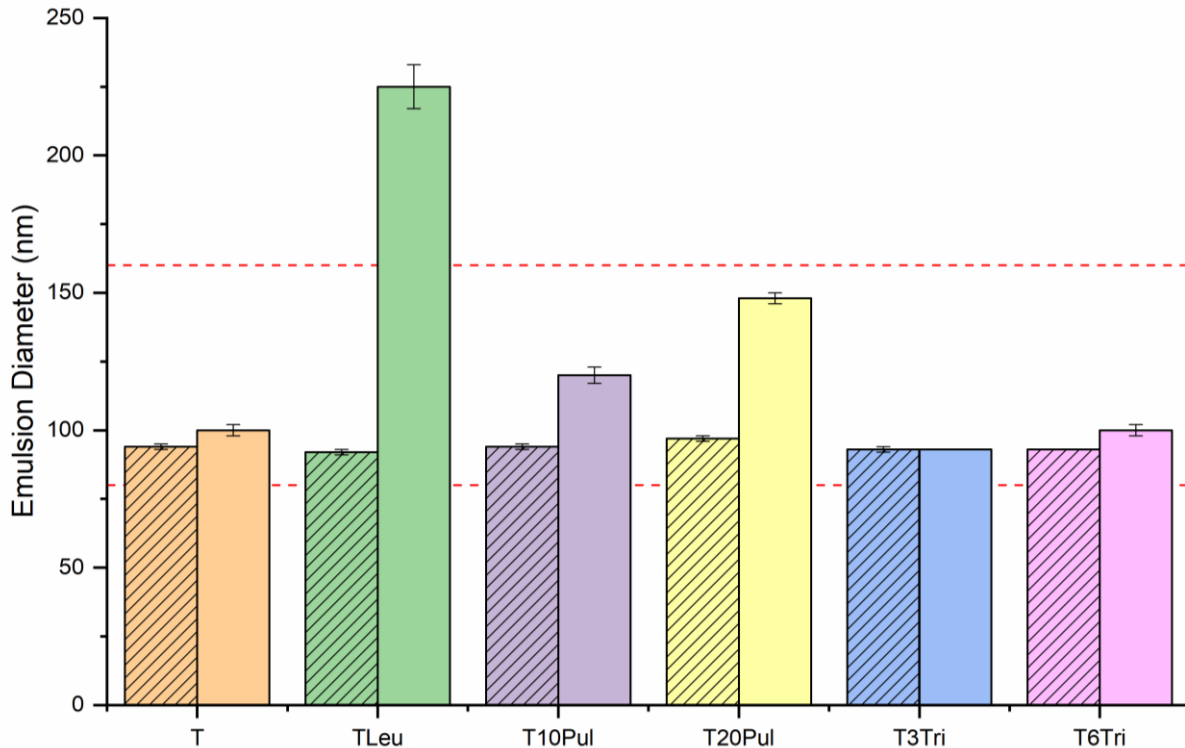
The vaccine nanoemulsion droplets' average diameter in the liquid formulation and reconstituted spray-dried powder are compared in Figure 5. The acceptable emulsion diameter range (80-160 nm) is represented by dashed red lines. The acceptance criteria are based on previously established quality control  
520 specifications for the nanoemulsion [69]. It is apparent that all formulations except T20Leu preserve emulsion diameter post-spray drying.

The trehalose control and both trileucine-containing formulations showed less than an 8% increase in emulsion diameter. These formulations had the highest relative mass fraction of trehalose, where trehalose composed 76-81% of the dry particles. High trehalose mass fraction increases the probability that the  
525 nanoemulsion droplets are surrounded by trehalose rather than other excipients. Similarly, a previous study involving spray-dried trehalose formulation at a higher feedstock concentration showed low increase in emulsion diameter of only 2-3% [23].

The T20Leu formulation's measured emulsion droplet diameter was the largest, increasing 145% to 225 nm. The significant increase in droplet diameter strongly suggests that leucine promotes instability of the  
530 GLA-SE membrane. The exhibited increase in emulsion diameter outside the acceptance limit removes the T20Leu candidate from consideration for further development. Crystallinity analysis results have shown that the leucine component in the T20Leu candidate is mostly crystalline. Studies on the lyophilization of the vaccine have shown that crystalline lyophilisate increased the GLA-SE particle size after reconstitution [22]. However, particle size analysis on a similar spray-dried formulation containing only 5% leucine mass

535 fraction also showed an increase in emulsion droplet diameter from 94 nm to 178 nm on reconstitution (data not shown). It is highly likely that the leucine component of this spray-dried formulation with such a low leucine mass fraction (<10%) is primarily amorphous, according to Feng et al.'s work [34]. Therefore, crystallization of leucine may not be the only mechanism which destabilizes the GLA-SE membranes. It has been established that leucine molecules are able to penetrate DMPC monolayers in aqueous solutions  
540 [70]. Penetration of the lipid layer by an amino acid has been previously reported to cause membrane destabilization on dehydration and subsequent reconstitution [71]. Despite the similar molecular structure of leucine and trileucine, the trileucine-containing formulations did not exhibit a large increase in emulsion diameter.

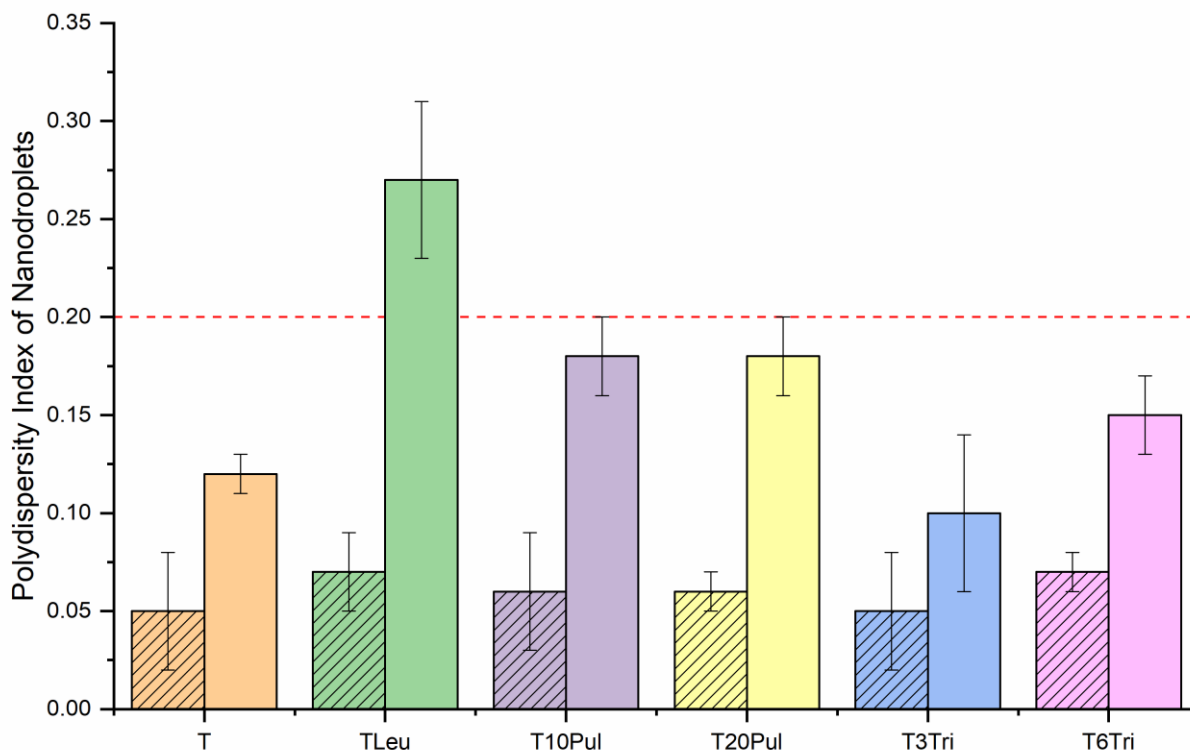
Spray drying the pullulan-containing formulations led to an increase in emulsion droplet diameter of 28%  
545 and 53%, for T10Pul and T20Pul respectively. The increase in diameter for the T10Pul formulation is comparable to the increase in GLA-SE diameter of the lyophilized vaccine [22]. Increasing pullulan concentration appears to cause greater increase in nanoemulsion droplet diameter on reconstitution. The particle formation model predicted that pullulan enriches the surface, however, the time to true density occurs near the same time for the trehalose component. Particle morphology of these formulations suggests  
550 that the particles are likely composed of a pullulan and trehalose mixture, as there is no clear distinction between the pullulan and trehalose layers. This distribution of components increases the likelihood of the emulsion droplets becoming encapsulated by pullulan, or a pullulan and trehalose mixture during drying. Addition of pullulan to stabilizing excipients has been previously shown to increase emulsion droplet size on reconstitution [72].



**Figure 5** Droplet diameter of the nanoemulsion before and after spray drying. Addition of pullulan appears to increase the average droplet diameter slightly. Inclusion of leucine greatly increased the droplet diameter. Trehalose-only and trileucine-containing formulations preserved the droplet diameter. Striped bars represent measurements on the liquid feedstock formulations. Solid bars represent measurements on the reconstituted spray-dried powders. Error bars represent the standard deviation of three measurements. Dashed red lines indicate the acceptance limits.

555 The polydispersity index of the nanoemulsion droplets in the liquid formulation and the reconstituted spray-dried powder for all inhalable vaccine candidates is shown in Figure 6. Maximum acceptable polydispersity index was limited to 0.2, as represented by the dashed red line. The results show that spray drying increased the polydispersity index of all inhalable vaccine candidates. This result is to be expected as some of the dispersed nanoemulsion droplets will inevitably collide and merge into larger ones during the spray drying

560 process, causing the size distribution to deviate from perfect monodispersity. However, the measured polydispersity index of all formulations, except for the T20Leu candidate, was within the preset target criteria (<0.2). Increased polydispersity index further suggests that leucine destabilized the emulsion membrane.



**Figure 6** Polydispersity index of the nanoemulsion droplets before and after spray drying for the inhalable vaccine candidates. The graph indicates that the polydispersity index increased for all formulations after spray drying. The leucine-containing formulation had a polydispersity index greater than 0.2 post-spray drying. Striped bars represent measurements on the liquid feedstock formulations. Solid bars represent measurements on the reconstituted spray-dried powders. Error bars represent the standard deviation of three measurements. Dashed red line indicates the acceptance limit.

### 565 3.4 Squalene and GLA Content

Comparison of squalene and GLA content between the feedstock and the reconstituted spray-dried powder for all inhalable candidates is shown in Table 4. Acceptance criteria was defined as  $\pm 20\%$  of the target squalene concentration (5.73 mg/mL) and the target GLA concentration (3.33  $\mu\text{g/mL}$ ). No decrease in squalene content was detectable for any formulation, suggesting successful encapsulation of nanoemulsion droplets during spray drying. Therefore, addition of the chosen dispersibility enhancing agents did not negatively affect the encapsulation efficiency. Additionally, the successful retention of squalene indicates

570

that the employed processing conditions were applicable for the different formulations. Reported higher values in squalene content after spray drying may be due to assay variability.

575 Similarly, it is apparent that no decrease in GLA content was detected for any formulation. The successful retention of GLA over spray drying suggests that the addition of the chosen dispersibility enhancing agents did not interfere with GLA stabilization via trehalose. Reported higher values in GLA content after spray drying may be due to assay variability.

**Table 4 Measured squalene and GLA content before and after spray drying for all inhalable candidates. All values are within 20% of the target.**

Formulations	Squalene Concentration (mg/mL)		GLA Concentration (µg/mL)	
	Liquid	Reconstituted Powder	Liquid	Reconstituted Powder
<b>Acceptance Limits</b>	4.58 - 6.88		2.66 – 4.00	
<b>T</b>	6.31 ± 0.12	6.27 ± 0.07	3.72 ± 0.08	3.77 ± 0.00
<b>T20Leu</b>	6.11 ± 0.06	6.35 ± 0.14	3.57 ± 0.02	3.73 ± 0.07
<b>T10Pul</b>	5.71 ± 0.08	6.10 ± 0.07	3.66 ± 0.02	3.77 ± 0.05
<b>T20Pul</b>	5.93 ± 0.07	6.21 ± 0.08	3.73 ± 0.01	3.83 ± 0.02
<b>T3Tri</b>	6.21 ± 0.02	6.42 ± 0.10	3.67 ± 0.02	3.83 ± 0.05
<b>T6Tri</b>	6.37 ± 0.11	6.89 ± 0.07	3.64 ± 0.04	3.52 ± 0.12

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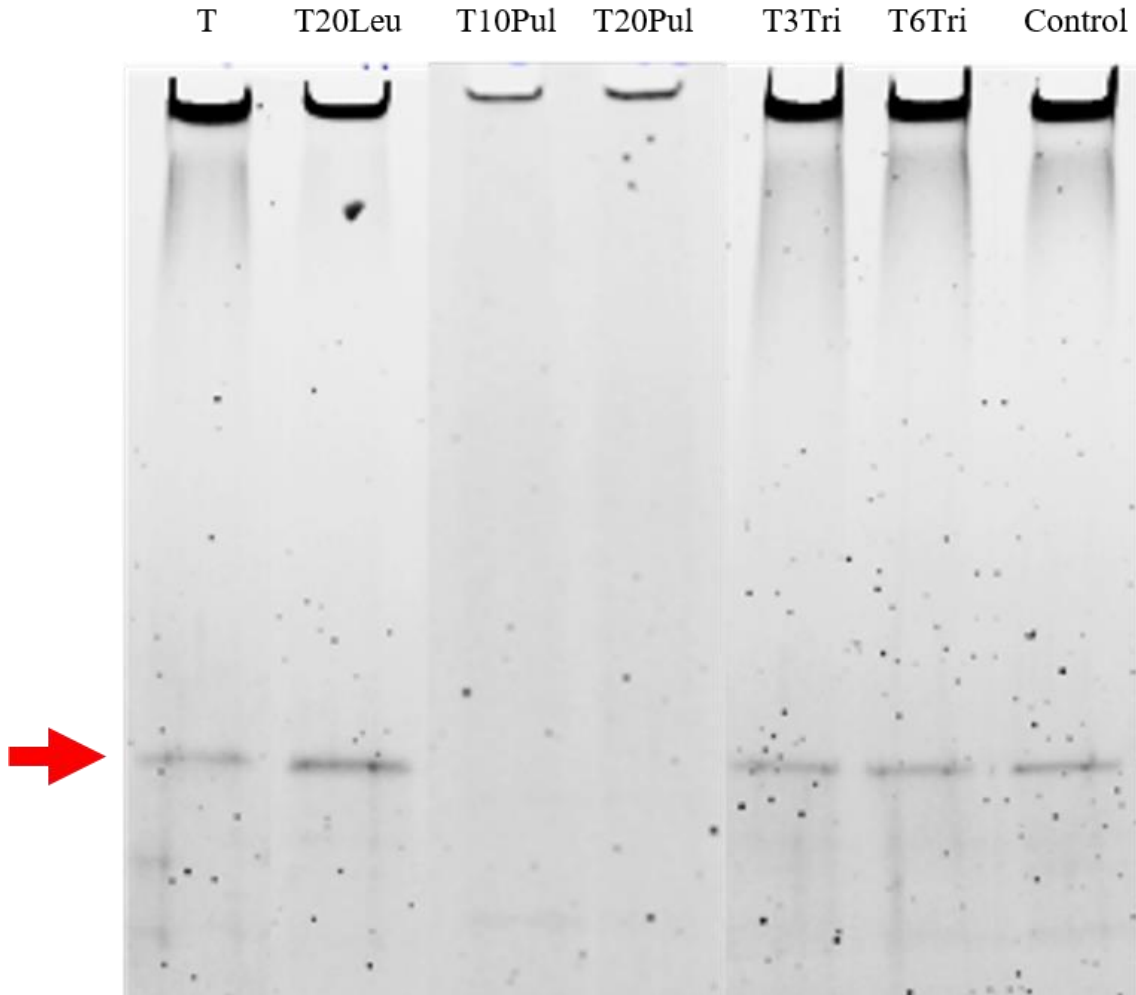
### 3.5 ID93 Retention

ID93 presence was measured using SDS-PAGE analysis. Stained gels of the inhalable vaccine candidates and a control are shown in Figure 7. The ID93 band was present in all formulations with the exception of those that contained pullulan.

585 The absence of an ID93 band in the T10Pul and T20Pul formulations suggests that the addition of pullulan negatively affects the formulations' ability to stabilize the ID93 protein, thus eliminating these formulations from consideration as inhalable candidates. Results were repeated for the pullulan-containing formulations (not shown) to confirm the absence of the ID93 band. Pullulan and trehalose excipient mixtures have successfully stabilized air-dried HSV-2 vaccine, however, pullulan alone has been shown to offer poor  
590 protection against desiccation, with significant loss in titer on drying and complete loss after only a week



of storage at room temperature [36]. Further investigation is required to determine why the ID93 band was not present in the pullulan-containing formulations.



**Figure 7** SDS-PAGE analysis for ID93 presence based on existence and location of band. Analysis was completed on all inhalable vaccine candidates. SDS-PAGE analysis for a control ID93+GLA-SE formulation has been provided in the last lane for comparison. Analysis indicates that the ID93 band is present for all formulations except those containing pullulan. Relative ID93 content among different formulations cannot be determined based on band intensity as the figure shown was combined from different imaged gels.

### 3.6 Aerosol Performance

Successful respiratory pharmaceutical delivery requires that an appropriate dose be delivered to the lung and that the powder deposits in the appropriate region of the lung. In this study, a throat model connected to an impactor was utilized to assess the dosage lost to mouth-throat deposition for each candidate under normal use. Lung dose was reported in this study rather than the commonly used measurement of fine

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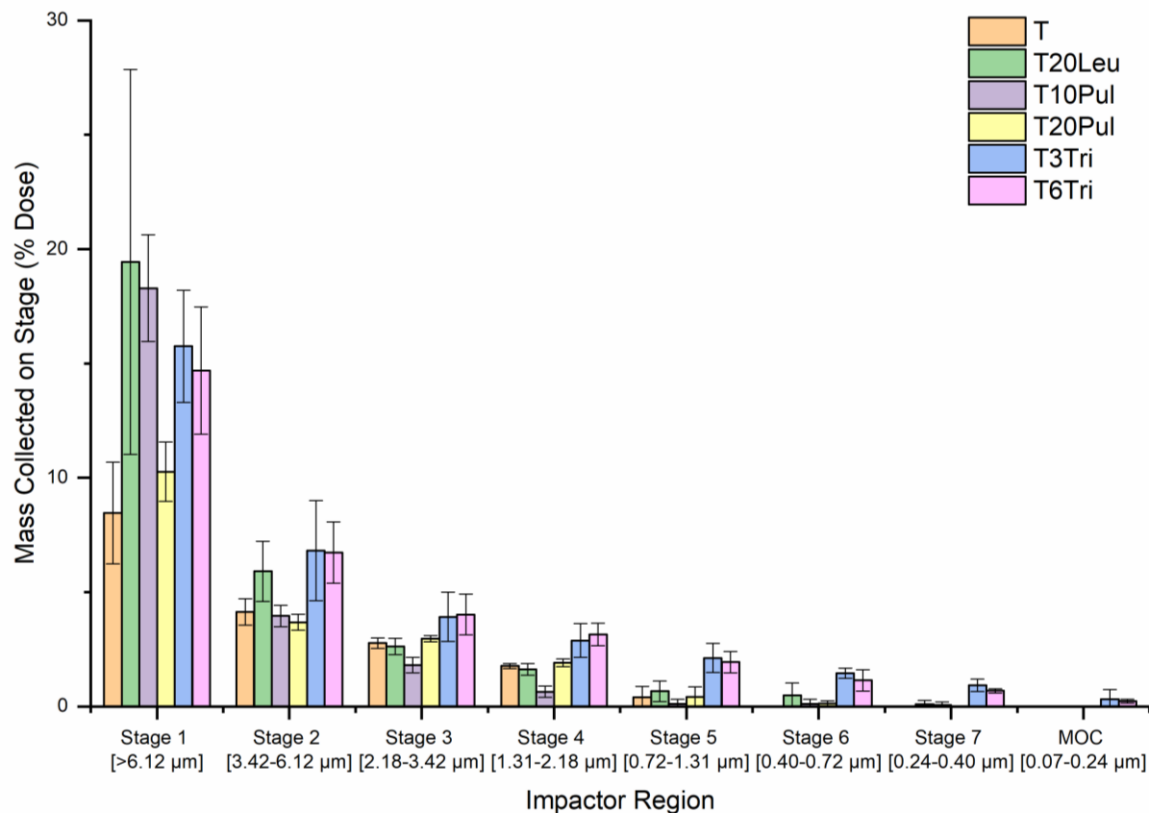
particle fraction, the fraction of deposited particles with a  $d_a \leq 5 \mu\text{m}$ . Fine particle fraction was not reported in this study as the set up utilized allows for the lung dose to be reported directly for a given candidate.

600 Table 5 compares the inhalable vaccine candidates' overall aerosol performance and size distribution of the lung dose, that is, the powder which penetrated the throat model and deposited within the impactor. Mass distribution of each candidate, shown in Figure 8, was used to calculate size distribution. The bracketed  $d_{a,50}$  values are greater than the minimum particle size expected to deposit on Stage 1 ( $6.12 \mu\text{m}$ ). The larger value indicates that these powders experienced greater deposition in the throat and on the first stage of the  
605 impactor due to significant particle aggregation.

Emitted dose for all inhalable candidates ranged from 84-97%. These results are very high for an experimental dry powder formulation, even outperforming some commercial DPI products [73]. However, the candidates exhibited markedly different performances in terms of lung dose.

610 **Table 5** Emitted dose, lung dose, and particle size analysis of the deposited powder for all inhalable vaccine candidates after aerosol performance experiments. Emitted dose was defined as the mass of powder that has left the DPI, and lung dose was defined as the mass of powder that penetrates the throat model. Both parameters are given as a percentage of the powder dose mass loaded into the capsules. Size distribution parameters  $d_{a,50}$  and  $\sigma_g$  were calculated via a fit to the cumulative lognormal distribution of the powder that deposited on the impactor stages. Results shown represent the average of triplicate measurements and error bars represent standard deviation. Statistically significant differences relative to the T formulation are marked with an asterisk. Bracketed values are greater than the Stage 1 cutoff diameter.  
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Formulation	Emitted Dose (% Dose)	Lung Dose (% Dose)	$d_{a,50}$ ( $\mu\text{m}$ )	$\sigma_g$
T	$87 \pm 13$	$18 \pm 0.5$	$5.7 \pm 0.8$	$2.3 \pm 0.1$
T20Leu	$97 \pm 3^*$	$32 \pm 12$	$(8.8 \pm 2.3)^*$	$2.9 \pm 0.6$
T10Pul	$89 \pm 13$	$25 \pm 3$	$(10.8 \pm 0.3)^*$	$2.5 \pm 0.3$
T20Pul	$84 \pm 12$	$19 \pm 2$	$(6.4 \pm 0.2)^*$	$2.6 \pm 0.3$
T3Tri	$93 \pm 15$	$34 \pm 6^*$	$5.7 \pm 0.2$	$4.2 \pm 1.5$
T6Tri	$96 \pm 6$	$33 \pm 6^*$	$5.4 \pm 0.2$	$3.4 \pm 0.4^*$



**Figure 8 Mass distribution of the inhalable vaccine powder for each formulation. Depth of penetration varied based on formulation composition. The trileucine-containing formulations had the greatest penetration, with deposition measured on the micro-orifice collector (MOC) of the impactor. Results shown represent the average of triplicate measurements and error bars represent standard deviation.**

The T formulation had the lowest mean lung dose of the investigated candidates. These results are expected as the T formulation did not include any dispersibility enhancing agents. The  $d_{a,50}$  of the T formulation was low compared to the other formulations, which would typically suggest that the formulation was well-dispersed. However, as shown in Figure 8, the T formulation deposited the lowest powder mass on Stage 1 as most of the powder aggregates deposited in the throat model instead. The lack of powder deposited on the later stages of the impactor further indicates that the T formulation was not well-dispersed. The low measured  $d_{a,50}$  is due to the much higher level of particle aggregation as compared to the others. The high level of aggregation led to most of the larger aggregates depositing in the throat prior to the impactor stages, as evidenced by the lowest lung dose.

The T20Leu formulation almost doubled lung dose as compared to the T formulation. This increase in aerosol performance was due to the designed rugose crystalline leucine surface layer of the T20Leu formulation, the presence of which was confirmed by morphology and solid state analysis. As discussed previously, increased rugosity and stiffness of the surface decreases the force of cohesion between particles and therefore make the powder more dispersible. These results showing that a crystalline leucine surface layer increases dispersibility of the powder was consistent with other studies. However, the fact that the measured  $d_{a,50}$  was higher than the theoretical values suggests that many particles remained aggregated after exiting the DPI. Feng et al. [34] demonstrated that increasing leucine concentration in spray-dried leucine-trehalose systems improves dispersibility of the powder. Similarly, Arora et al. [74] demonstrated that spray drying the drug voriconazole with 20% leucine increased dispersibility when tested using a similar DPI and NGI set up. Emitted dose for the spray-dried voriconazole formulation without leucine was only 58% but increased to 82% for the formulation containing 20% leucine. However, the dispersibility of a crystalline formulation is not solely dependent on the presence of surface crystals but also on their size and the number density of these surface crystals. Raula et al. [75] coated salbutamol sulphate microparticles with leucine at different saturation levels and assessed dispersibility of the powders using a commercial DPI with a custom inhalation simulator. Morphological analysis found that increasing leucine content led to an increase in size and number density of asperities on the surface of the particles. The leucine coating improved particle dispersity over the uncoated particles, however, the authors found that the emitted dose decreased with further increasing leucine content. Smaller surface asperities may be more beneficial for improving particle dispersity as larger surface asperities may not reduce contact area and instead introduce mechanical interlocking forces between particles.

Neither of the pullulan-containing formulations improved lung dose significantly as compared to the T formulation. Particle surface morphology analysis showed that the addition of pullulan produced dented particles that still maintained an overall smooth surface. The dented surface morphology did not sufficiently reduce the forces of cohesion between the particles. The particle surface dimples may have been detrimental

in the present study due to the polydispersity of the powder as it is possible that the dimples in the larger particles may have provided an area for smaller particles to settle into, increasing the contact area between the two. Similarly, the measured particle sizes, which were larger than the theoretical predictions, also suggest a high level of particle aggregation. Particle dimples are shown to a higher extent with increased pullulan concentration, possibly explaining the lower aerosol performance of the T20Pul formulation compared to T10Pul. Previously, Carrigy et al. [41] showed that spray-dried pullulan-trehalose systems at different concentrations either improved or had the same aerosol performance as spray-dried trehalose microparticles. Their results found that a formulation containing 10% pullulan and 90% trehalose by mass improved the aerosol performance compared to spray-dried trehalose alone, however, a 40% pullulan and 60% trehalose formulation had an aerosol performance similar to that of trehalose alone. This suggests a point of diminishing returns for the addition of pullulan to improve powder dispersibility.

It is apparent that the trileucine-containing formulations, T3Tri and T6Tri, performed the best out of the tested inhalable vaccine candidates. These formulations were the only ones found to significantly improve the mean lung dose as compared to the T formulation. The measured 33-34% lung dose of these formulations is comparable to the lung dose obtained with commercial products. Ruzycski et al. [76] found that the lung dose, as a percentage of label claim, of six commercial DPI's ranged from 19-35% at the minimum efficacious flow rate and 22-53% at a standard pressure drop. Similarly, the Borgstrom et al. [77] found that lung dose of two commercial Turbuhaler DPIs in asthmatic patients averaged 20.8% and 16.9%. The measured  $d_{a,50}$  for the trileucine-containing formulations was also the lowest out of all inhalable candidates. The average  $\sigma_g$  values of the trileucine-containing formulations were the largest, indicating a wide range in particle size of the deposited powder. The dispersed powder size range is illustrated in Figure 8 where the trileucine containing formulations were the only candidates to exhibit powder deposition on all NGI stages and the MOC. Altogether, these results indicate that the inclusion of trileucine led to superior ability to disperse the smaller particles in the powder.

675 The addition of trileucine produced the greatest change in particle morphology, where analysis indicated the production of large particles that were outside the intended size range. However, the SEM images showed that these particles are thin-shelled and hollow; this morphology suggests that the particles have low density and therefore, the aerodynamic diameter of the particles is much smaller than the geometric diameter. Powders composed of geometrically large particles are easier to disperse as the aerodynamic  
680 forces, which act to disperse the powder during inhalation, increase with increasing particle diameter [27]. Additionally, the designed wrinkled surface morphology due to trileucine surface accumulation decreases contact area between particles, theoretically improving powder dispersibility. Accumulation of trileucine on the particle surface is also expected to reduce surface energy. Previously, increased trileucine content has been shown to improve powder dispersibility through reduction of particle surface energy even when  
685 particle morphology was no longer changing with increasing concentration [39]. These factors likely all contributed to the improved aerosol performance of the trileucine-containing formulations in this study. Based on the high dispersibility potential, the trileucine-containing formulations are the only ones which can deliver a portion of the vaccine in the peripheral region of the lung. Differences in the aerosol performance of the T3Tri and the T6Tri formulations were statistically insignificant, suggesting a similar  
690 level of trileucine particle surface coverage for both the T3Tri and the T6Tri formulations.

None of the inhalable vaccine candidates was completely dispersed to the predicted primary aerodynamic particle size of 3-4  $\mu\text{m}$ . However, aerosol performance assessment was completed with an unoptimized DPI in this study. As explicitly noted in de Boer et al.'s [73] review paper on dry powder inhalation, successful pulmonary delivery of vaccines often requires further DPI development to improve efficiency and deep  
695 lung delivery. Recently, Sibum et al. assessed the aerosol performance and stability of isoniazid spray-dried with leucine or trileucine [78]. Their results found that use of the Cyclops DPI over a Twincer DPI improved the emitted dose of the 3% leucine, 5% leucine, and 3% trileucine formulations by approximately 40%, 25%, and 10%, respectively.

## 4 Conclusion

700 This study demonstrates the use of particle engineering principles in the investigation of various excipients to improve aerosol performance of a complex inhalable vaccine formulation. In this study an excipient system was developed that encapsulated an adjuvanted subunit TB vaccine candidate formulated as a nanoemulsion via spray drying. Results found that the adjuvant system was successfully stabilized, with evidence shown that the antigen is present in the spray dried powder. Promising aerosol performance was  
705 achieved by adding a dispersibility enhancer, trileucine, to the formulation. This study also demonstrated the potential of the vaccine to be delivered as a respirable dosage to human lungs via inhalation using a DPI. Published work on spray drying vaccines formulated as lipid-based dispersions has primarily focused on stabilization.

The demonstrated potential for pulmonary vaccine delivery creates options for vaccines, such as the model  
710 TB vaccine investigated in this study, to be administered via an alternative route to traditional parenteral injection. Intranasal delivery of the spray-dried vaccine may be possible with adjustments to some particle properties, such as the size of the spray-dried particles, or switching to another delivery device. Administration through inhalation mitigates risks associated with needle delivery such as needlestick injuries, needlestick waste, and transfer of bloodborne illnesses. Nevertheless, more work is needed to  
715 further characterize the storage stability of the inhalable spray-dried vaccine. Additionally, while the potential for pulmonary delivery has been demonstrated at this point it is not known which administration route will elicit the strongest immune response for this particular TB vaccine candidate. Preclinical *in vivo* studies must be completed to compare the effects of vaccine administration via different routes on immunogenicity and efficacy.

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